

ASSESSING THE ECONOMIC IMPACT OF CO₂ CAPTURE AND RES-H₂ PROCESSES ON THE FEASIBILITY OF OLEFINS PRODUCTION

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ABSTRACT

Anthropogenic greenhouse gas emissions are the main contributors to the climate change, causing a rise in global temperature and catastrophic weather effects. Among them, CO₂ is emitted from a series of activities that involve the use of fossil fuels in power plants, heavy industrial units (e.g. cement, steel) and in transportation sector. To this end, the deployment of CO₂ capture and utilization (CCU) strategies along with the use of green H₂ can provide a valorization pathway to value-added products, such as methanol, olefins, formic acid, etc. Among the various products, light olefins are vital chemicals extensively employed as a building block for numerous petrochemical products (plastics, textiles, rubbers, etc.).

In view of the above aspects, the present work aims to assess an industrial scale process for the production of C₂-C₄ olefins under zero C-emissions and market-competitive prices. The proposed study will include the following step-by-step assessment:

- *Simulation, process design and economic evaluation of a CO₂ capture process through MEA.*
- *Optimal design, energy management and economic evaluation of a RES-H₂ production system based on solar/wind energy and PEM electrolysis.*
- *Preliminary analysis on the design of a flexible catalytic process that will be able to combine two high purity streams (CO₂+H₂) towards the production of olefins in multi-step reactors and purification units.*

Specifically, ASPEN PLUS will be used to simulate the CO₂ capture process through the use of MEA in a consequent absorption-desorption cycle. Heat exchange is highly important and will be fully considered in our study. The proposed process will aim at the processing of a complete flue gas exit stream from a cement factory (~10,000ktn/yr) and will be economically evaluated targeting a price range of 40-70€/tn for the captured CO₂. In parallel, the optimal design and simultaneous energy management of H₂ production from solar and wind energy will take place for a continuous production rate (~300ktn/yr) and will target a price range of 10-20€/kg of H₂ (excluding transportation costs). The above analysis will be used to retrofit the preliminary study of scaled-up olefins production in a catalytic reactor and purification process and will be compared with conventional olefin production in petrochemical industries.

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